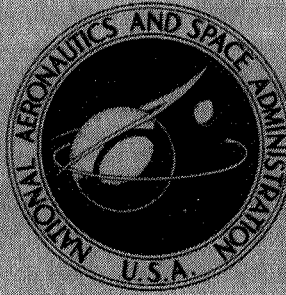


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**COMPUTER PROGRAM TO CALCULATE  
CONVECTIVE HEAT-TRANSFER COEFFICIENTS  
FROM HARMONIC TEMPERATURE OSCILLATIONS**

*by Geraldine E. Amling and Ronald G. Huff*

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# COMPUTER PROGRAM TO CALCULATE CONVECTIVE HEAT-TRANSFER COEFFICIENTS FROM HARMONIC TEMPERATURE OSCILLATIONS

by Geraldine E. Amling and Ronald G. Huff

Lewis Research Center

## SUMMARY

Two FORTRAN IV version 13 programs are described which obtain the analytical solutions for convective heat-transfer coefficients related to either the phase lag or the amplitude ratio. The first, entitled BL, uses the ratio of the wall to driven hot fluid temperature to calculate the coefficients. The second, entitled JCL, uses the phase-lag angle between the sinusoidally driven fluid and wall temperature to calculate the heating fluid and coolant convective coefficients. Criteria for the choice of either of the two methods and their mathematical formulation are described in detail in reference 1.

## INTRODUCTION

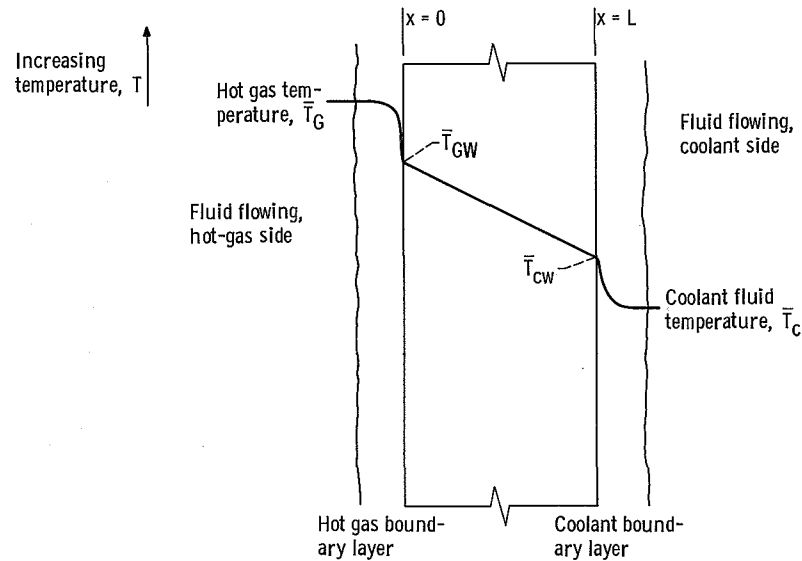
The analytical expressions to determine the convective heat-transfer coefficients for a wall separating two fluids, one having an oscillating temperature, were derived in reference 1 from a second-order partial differential equation. These equations lead to computational procedures that are iterative and, therefore, time consuming and tedious. To alleviate this difficulty, two computer programs, BL and JCL, were written to provide the means for obtaining the numerical solutions to either the amplitude ratio or the phase-lag angle method quickly and accurately.

The data published in reference 1 were obtained by the use of these programs, and their descriptions and listings, which are shown herein, should prove helpful to anyone desiring to investigate further.

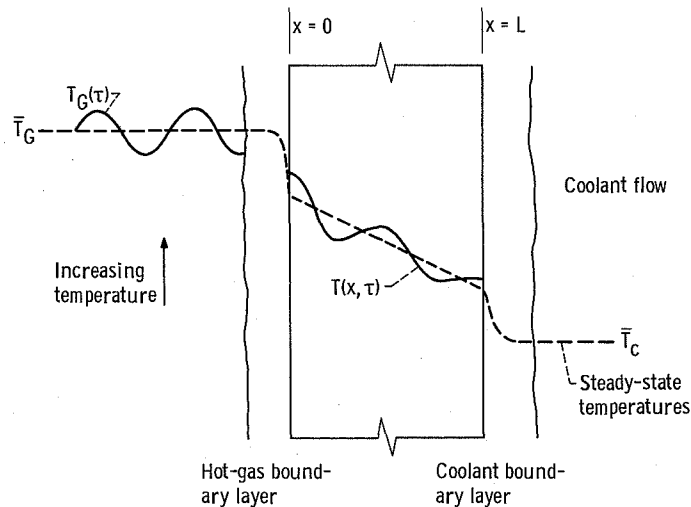
Specifically, the BL program calculates the convective heat-transfer coefficients related to the amplitude ratio for a plate separating two fluids, one of the fluids having an oscillating temperature. The JCL program, on the other hand, calculates the heat-transfer coefficients related to the phase lag.

## STATEMENT OF THE PROBLEM

Figure 1(a) shows a wall that separates two moving fluids. The hot-gas-side fluid temperature  $T_G$  is greater than the coolant temperature  $T_c$ , causing heat to flow through the wall in the positive  $x$  direction. The problem is to determine the convective heat-transfer coefficients if either the hot-gas or coolant temperature is varied sinusoidally and if the temperature response of the wall is measured at only one point. Figure 1(b) shows what the wall temperature might look like at any given instant in time.



(a) Wall temperature distribution shown at time zero before start of hot-gas temperature oscillation.



(b) Transient temperature response of plate to sinusoidally forced fluid temperature.

Figure 1. - Basic heat-transfer model.

## METHOD OF ATTACK

If the hot-gas temperature is made to vary sinusoidally, the wall temperature will respond sinusoidally but will lag the driven temperature by an angle  $\varphi$ . In addition, the amplitude of the wall temperature oscillation will be less than that of the driven temperature. Both the phase lag  $\varphi$  and the ratio of the amplitude of the wall temperature to the amplitude of the driven temperature  $\theta/\Delta T$  are, among other things, functions of the convective heat-transfer coefficients  $h$ . Finding the relation between the convective heat-transfer coefficients and the phase lag  $\varphi$ , or the amplitude ratio  $\theta_m/\Delta T$ , is required in order to solve for the coefficients.

To find this relation, the temperature response of the wall to a sinusoidally driven fluid temperature is derived. From this solution and steady-state heat-transfer conditions (which relate the ratio of the convective heat-transfer coefficients to the ratio of the temperature drops between fluids and wall), the absolute values of the coefficients can be determined as functions of either phase lag or amplitude ratio. The quantities that must be known as a function of time are the hot-gas temperature  $T_G$ , the wall temperature at any point  $x$  ( $T(x, \tau)$ ) and the coolant temperature  $T_c$ . From these quantities either the phase lag or the amplitude ratio can be determined as well as the ratio of the convective heat-transfer coefficients. With the ratio of the coefficients, the frequency of the temperature oscillation, the wall material properties, and either  $\varphi$  or  $\theta_m/\Delta T_G$ , the convective heat-transfer coefficients  $h_G$  and  $h_c$  can be calculated.

It is also possible to calculate the coefficients by oscillating the coolant temperature sinusoidally. This approach requires the measurement of the same quantities as when the hot fluid temperature is oscillated.

The controlling differential equations and boundary conditions are given next. The one-dimensional transient heat-conduction equation<sup>1</sup>

$$\frac{\partial^2 T}{\partial x^2} = \frac{1}{\alpha} \frac{\partial T}{\partial \tau} \quad (1)$$

is solved for the temperature distribution in a wall that has convective heat transfer over its two surfaces (fig. 1). (Symbols are defined in the appendix.) The hot-gas side fluid temperature is driven sinusoidally and is given in equation form by

$$T_G = \Delta T_G e^{-i\omega\tau} + \overline{T}_G \quad (2)$$

---

<sup>1</sup>All equations are numbered to correspond with those in reference 1.

where  $\bar{T}_G$  is given. It is not necessary to know the numerical value of  $\Delta T_G$  if the phase lag is used for calculating the coefficients because the phase determination is independent of the absolute value of the temperature oscillation. If the amplitude ratio is used for calculating the coefficients, the  $\Delta T_G$  must be computed from the change in chamber pressure. The boundary condition at the hot-gas side of the wall surface  $x/L = 0$  equates the heat transferred by convection to that conducted away from the surface into the wall. This is given in equation form as

$$h_G [T_G - T(0, \tau)] = -K \frac{\partial T(0, \tau)}{\partial x} \quad (3)$$

The boundary condition at the coolant surface ( $x/L = 1$ ) equates the heat conducted to the surface with the heat transferred convectively to the coolant. In equation form this is given by

$$h_c [T(L, \tau) - T_c] = -K \frac{\partial T(L, \tau)}{\partial x} \quad (4)$$

The solution for the wall temperature as a function of time and location within the wall consists of the sum of the transient  $\theta(x, \tau)$  and steady-state  $T_s(x)$  solutions. The steady-state solution is found by setting  $\partial T / \partial \tau$  equal to zero in equation (1) and assuming the wall temperature at  $x/L = 0$  and 1 to be given as  $T_{GW}$  and  $T_{cw}$ , respectively. This yields the usual linear temperature distribution with distance and can be written as

$$\bar{T}_s(x) = (\bar{T}_{cw} - \bar{T}_{GW}) \frac{x}{L} + \bar{T}_{GW} \quad (5)$$

The transient solution  $\theta(x, \tau)$  is found by assuming the usual product solution: one a function of time only  $F(\tau)$  and the other a function of the location within the wall measured from the heated side of the wall  $X(x)$ . Equations (1), (3), and (4) are modified to account for the change in variable from  $T(x, \tau)$  to  $\theta(x, \tau)$ . The details of the solution of equation (1) using its pertinent boundary conditions (eqs. (2) to (4)) are shown in appendix B of reference 1.

The relation, derived from the steady-state (or mean) condition that requires the heat transferred convectively to the wall to equal the heat transferred convectively to the coolant, is expressed mathematically as



$$\frac{h_c}{h_G} = \frac{\overline{T}_G - \overline{T}(0)}{\overline{T}(L) - \overline{T}_c} \quad (6)$$

From the definition of  $\psi$

$$h = \frac{K\eta}{\psi} \quad (7)$$

The ratio of convective heat-transfer coefficients in equation (6) is defined as  $R$ . Calculating the ratio  $R$  using equation (7) gives

$$R = \frac{\psi_G}{\psi_c} \quad (8)$$

where  $R$  is also given by

$$R = \frac{\overline{T}_G - \overline{T}(0)}{\overline{T}(L) - \overline{T}_c} \quad (9)$$

The following assumptions have been used to obtain the solution:

- (1) The heat flows through the plate in the  $x$  direction only (one-dimensional heat conduction).
- (2) The wall or plate properties (density, specific heat, and thermal conductivity) are constant.
- (3) The convective heat-transfer coefficients on both sides of the wall are constant.
- (4) The coolant temperature is constant.

The details of the analytical solutions are given in reference 1. However, the following equations are restated herein because they are used by the computer program to calculate the heat-transfer coefficients.

The equation involving amplitude ratio is

$$\frac{\theta_m}{\Delta T_G} = \frac{1}{a^2 + b^2} \left( \left\{ \left[ (ca - db) \sin \eta L \frac{x}{L} - (da + cb) \cos \eta L \frac{x}{L} \right] e^{\eta L [2 - (x/L)]} + \left[ (fa - eb) \cos \eta L \frac{x}{L} - (ea + fb) \sin \eta L \frac{x}{L} \right] e^{\eta L (x/L)} \right\}^2 \right. \\ \left. + \left\{ \left[ (ea + fb) \cos \eta L \frac{x}{L} + (fa - eb) \sin \eta L \frac{x}{L} \right] e^{\eta L (x/L)} - \left[ (ca - db) \cos \eta L \frac{x}{L} + (da + cb) \sin \eta L \frac{x}{L} \right] e^{\eta L [2 - (x/L)]} \right\}^2 \right)^{1/2} \quad (B37)$$

where

$$a = 1 - (\psi_G + \psi_c) + e^{2\eta L} \left[ (\psi_G + \psi_c + 2\psi_G \psi_c) \sin 2\eta L - (1 + \psi_c + \psi_G) \cos 2\eta L \right] \quad (B28)$$

$$b = (\psi_G + \psi_c - 2\psi_G \psi_c) + e^{2\eta L} \left[ (\psi_G + \psi_c + 2\psi_G \psi_c) \cos 2\eta L + (1 + \psi_c + \psi_G) \sin 2\eta L \right] \quad (B29)$$

$$c = (1 + \psi_c) \cos 2\eta L - \psi_c \sin 2\eta L \quad (B30)$$

$$d = \psi_c \cos 2\eta L + (1 + \psi_c) \sin 2\eta L \quad (B31)$$

$$e = 1 - \psi_c \quad (B32)$$

$$f = \psi_c \quad (B33)$$

The equation involving phase lag angle is

$$\psi_c^3 + \frac{[\underline{C} + R(\underline{C} + D)]}{R(F + G)} \psi_c^2 + \frac{2\underline{A} + R(\underline{A} + \underline{B})}{2R(F + G)} \psi_c + \frac{E}{2R(F + G)} = 0 \quad (B51)$$

where

$$\begin{aligned} \underline{A} \equiv & -\sin(\varphi + \eta x) + e^{2\eta L} \cos(\varphi + \eta x - 2\eta L) + e^{2\eta(2L-x)} \sin(\varphi - \eta x) \\ & - e^{2\eta(L-x)} \cos(\varphi - \eta x + 2\eta L) \end{aligned} \quad (B39)$$

$$\begin{aligned} \underline{B} \equiv & \cos(\varphi + \eta x) - e^{2\eta L} \sin(\varphi + \eta x - 2\eta L) - e^{2\eta(2L-x)} \cos(\varphi - \eta x) \\ & + e^{2\eta(L-x)} \sin(\varphi - \eta x + 2\eta L) \end{aligned} \quad (B40)$$

$$\begin{aligned} \underline{C} \equiv & \sin(\varphi + \eta x) + e^{2\eta L} \sin(\varphi + \eta x - 2\eta L) + e^{2\eta(2L-x)} \sin(\varphi - \eta x) \\ & + e^{2\eta(L-x)} \sin(\varphi - \eta x + 2\eta L) \end{aligned} \quad (B41)$$

$$\begin{aligned} \underline{D} \equiv & -\cos(\varphi + \eta x) + e^{2\eta L} \cos(\varphi + \eta x - 2\eta L) - e^{2\eta(2L-x)} \cos(\varphi - \eta x) \\ & + e^{2\eta(L-x)} \cos(\varphi - \eta x + 2\eta L) \end{aligned} \quad (B42)$$



$$E \equiv \sin(\varphi + \eta x) - e^{2\eta L} \sin(\varphi + \eta x - 2\eta L) + e^{2\eta(2L-x)} \sin(\varphi - \eta x) - e^{2\eta(L-x)} \sin(\varphi - \eta x + 2\eta L) \quad (B43)$$

$$F \equiv \cos(\varphi + \eta x) + e^{2\eta L} \sin(\varphi + \eta x - 2\eta L) - e^{2\eta(2L-x)} \cos(\varphi - \eta x) - e^{2\eta(L-x)} \sin(\varphi - \eta x + 2\eta L) \quad (B44)$$

$$G \equiv -\sin(\varphi + \eta x) - e^{2\eta L} \cos(\varphi + \eta x - 2\eta L) + e^{2\eta(2L-x)} \sin(\varphi - \eta x) + e^{2\eta(L-x)} \cos(\varphi - \eta x + 2\eta L) \quad (B45)$$

The solution of this cubic equation can be obtained using the classical approach. The positive, nonzero, root will yield the desired convective heat-transfer parameter  $\psi_c$ . From equation (8), then

$$\psi_G = R\psi_c \quad (B52)$$

Also, from equations (6) and (9), the following relation must be satisfied:

$$R \equiv \frac{h_c}{h_G} = \frac{T_G - T(0)}{T(L) - T_c} \quad (B49)$$

## DESCRIPTION OF BL AND JCL

The computer program, BL, was written to calculate the heat-transfer coefficients  $h_c$  and  $h_G$  by use of values of the thermal conductivity  $K$ , the density of the wall material  $\rho$ , the specific heat of the wall material  $c$ , thickness of wall material  $L$ , the ratio of distance measured from the heated surface wall to the thickness of the wall  $x/L$ , the mean temperature of the hot gas  $\bar{T}_G$ , the wall temperature as a function of time at  $x = 0$   $T(0, \tau)$ , the mean temperature of the coolant  $\bar{T}_c$ , the frequency of temperature oscillation  $f$ , and the amplitude ratio  $\theta/\Delta T_G$ .

The coolant wall temperature  $T_{cw}$  is initially set to a positive perturbation value in subroutine BALAN for the coolant temperature  $\bar{T}_c$ . The ratio of the convective heat-transfer coefficients  $R$ , is then calculated, and with a linear relation of conductive heat transfer across the plate both heat-transfer coefficients  $h_c$  and  $h_G$  can be obtained. With these quantities, a calculated amplitude ratio is found and compared with the meas-

ured ratio. Then, by means of linear interpolation in subroutine BALAN,  $T_{cw}$  is altered until the difference between the two ratios is less than  $10^{-4}$ .

It should be noted that the  $\theta/\Delta T_G$  ratio as a function of the coolant wall temperature has a pole at  $T(x, \tau)$  (fig. 2), which imposes a heavy restriction on the allowable error for the value of the amplitude ratio. If the error in the amplitude ratio exceeds 10 percent of the true value, the iteration will converge to a value for the coolant wall temperature in excess of the gas wall temperature.

The computer program JCL was written to calculate heat-transfer coefficients  $h_c$  and  $h_G$  by use of values of the thermal conductivity  $K$ , the density of wall material  $\rho$ , the specific heat of wall material  $c$ , thickness of wall material  $L$ , the ratio of distance measured from the heated surface of the wall to the thickness of the wall  $x/L$ , the mean temperature of the hot gas  $\bar{T}_G$ , the wall temperature as a function of distance (measured into wall from hot surface)  $T(x, \tau)$ , the mean temperature of the coolant  $\bar{T}_c$ , the frequency of temperature oscillation  $f$ , and the phase lag angle  $\theta$ . The coolant wall temperature  $T_{cw}$  is initially set to equal the measured temperature of the wall  $T(x, \tau)$ . The ratio  $R$ , of the convective heat-transfer coefficients is calculated, and the coolant wall temperature value is corrected for the wall temperature drop due to conduction. Only the positive, nonzero root is used when solving the cubic equation.

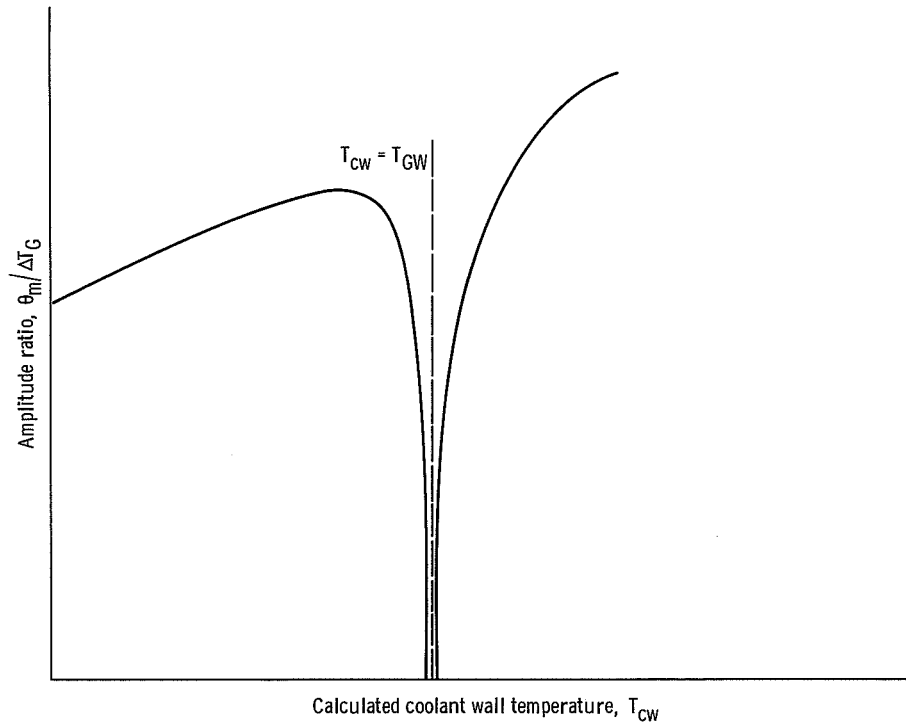


Figure 2. - Typical variation of amplitude ratio versus coolant wall temperature  $T_{cw}$  showing singularity at  $T_{cw} = T_{GW}$ .

These programs assume that the hot-gas-side temperature is measured. Therefore, the coolant wall temperature is calculated from the following equation:

$$T_{cw} = T(x, \tau) - \frac{(h_G)(L) [\bar{T}_G - T(x, \tau)]}{K}$$

If the wall temperature is measured at a point other than the hot-gas surface  $x/L \approx 0$ , the programs must be modified to account for the new location.

## INPUT CARDS

### Program BL

The BL program requires the following cards for input information:

Card 1: Three values with 3I2 format (table I, line 1) containing

IRDG reading number  
 ISTA station number  
 NR number of readings to be processed

Card 2: Nine values with 10E8.4 format (table I, line 2) containing

K conductivity  
 RHO density of wall material  
 CC specific heat of wall material  
 L thickness of wall material  
 XL ratio of distance measured from hot-gas side of wall and temperature measuring location to wall thickness  
 TG mean temperature of hot gas  
 TWO wall temperature, a function of time, at  $x = 0$   
 TWL wall temperature, a function of time, at  $x = L$   
 TC mean temperature of coolant

Card 3: Contains pairs of values (table I, line 3) under 10E8.4 format showing

WRAD(1) frequency of temperature oscillation  
 OMDTG(1) ratio of amplitude of wall temperature oscillation to amplitude of sinusoidally driven hot-gas temperature

.  
 .  
 .

OMDTG(NR)

The program read in NR pairs of values, up to five pairs in card 3. If more than five pairs are desired, more cards may be added. The NR pairs will continue to be read under the same 10E8.4 format.

TABLE I. - SAMPLE INPUT FOR PROGRAM BL

[illegible]

## Program JCL

The JCL program requires the following cards for input information:

Card 1: Three values with 3I2 format (table II, line 1) containing

IRDG	reading number
ISTA	station number
NR	number of readings to be processed

Card 2: Eight values with 10E8.4 format (table II, line 2) containing

K	conductivity
RHO	density of wall material
CC	specific heat of wall material
L	thickness of wall material
XL	ratio of distance measured from hot-gas side of wall and temperature measuring location to wall thickness
TG	mean temperature of hot gas
TGW	wall temperature, a function of distance
TC	mean temperature of the coolant

Card 3: Contains pairs of values (table II, line 3) under 10E8.4 format showing

WRADA(1)	frequency of temperature oscillation
PHIRA(1)	phase lag angle between driving gas temperature and responding wall temperature

PHIRA(NR)

TABLE II.. - SAMPLE INPUT FOR PROGRAM JCL

[illegible]

The outputs of both BL and JCL programs display the descriptive title followed by a list of the input values with their program labels. The results of the calculations appear under the heading OUTPUT shown in the next sections.

TCWA	calculated coolant wall temperature
TEST1	heat flux to coolant
TEST2	heat flux from hot gas
TEST	ratio of heat flux to coolant to heat flux from hot gas (ideally should be 1.0)
HCT	time averaged convective heat-transfer coefficient on coolant side of wall
HGT	time averaged convective heat-transfer coefficient on hot-gas side of wall
ERROR	(1.0 - TEST) which is used by the program to test against the convergence criterion
R	ratio of convective heat-transfer coefficients
THETA	final calculated value of ratio of the amplitude of wall temperature to amplitude of sinusoidally driven hot-gas temperature

## Program JCL

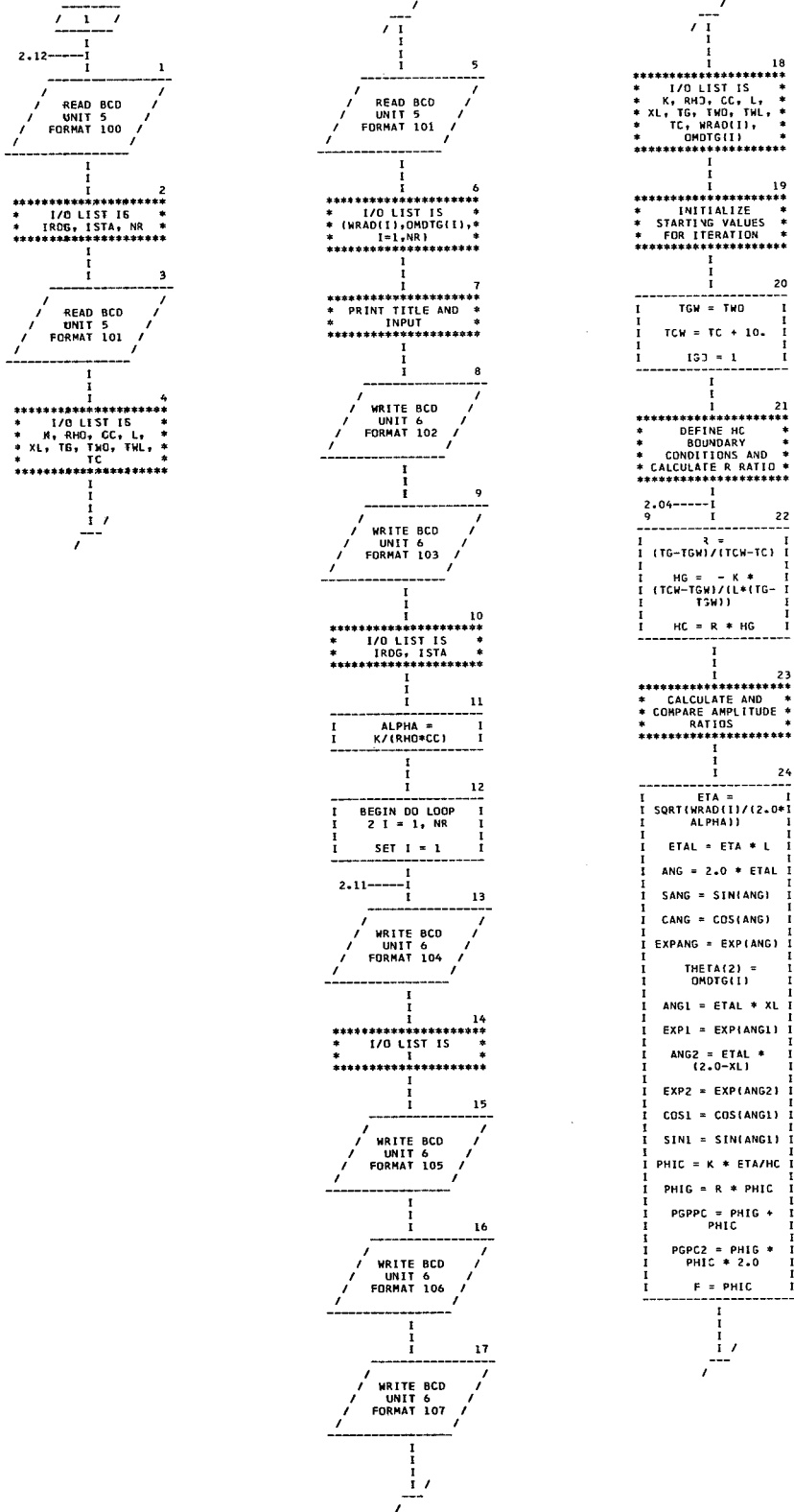
TCW	calculated coolant wall temperature
TEST1	heat flux to coolant
TEST2	heat flux from hot gas
TEST	ratio of heat flux to coolant to heat flux from hot gas (ideally should be 1.0)
HCT	time averaged convective heat-transfer coefficient on coolant side of wall
HGT	time averaged convective heat-transfer coefficient on hot gas side of wall
ERROR	(1.0 - TEST) which is used by the program to test against convergence criterion
R	ratio of convective heat-transfer coefficients
PSIC	convective heat-transfer parameter on coolant side of wall
PSIG	convective heat-transfer parameter on hot-gas side of wall
GR	check on the zero of eq. (B51) which should be equal to 0.0000

## COMPUTER PROGRAMS

These programs are written in FORTRAN IV and are operational on the IBM 7094-2/7044 direct-coupled system of the Lewis Research Center. Program BL uses approximately 5187)<sub>10</sub> storages and Program JCL uses approximately 4261)<sub>10</sub> storages. Flow charts of the programs are shown in figures 3 and 4.

Machine running time for both programs is minimal, each using less than 1 minute per case.

PROGRAM BL - AMPLITUDE RATIO GIVEN



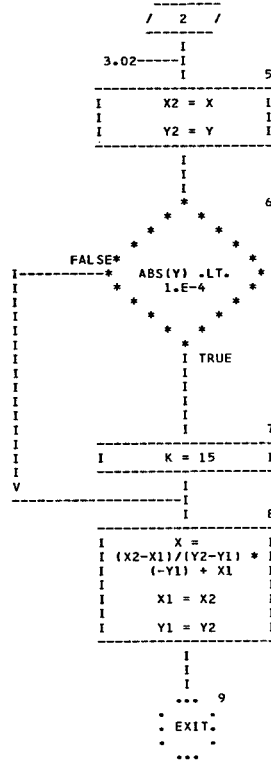




```

      / 1 /
      |
3.02----|
      |
-----
I      X1 = X      I
I      Y1 = Y      I
I      X = X + X/10. I
I      K = 2      I
-----
      |
      |
      |
      ... 4
      .
      . EXIT .
      .

```



```

C      L=THICKNESS OF WALL MATERIAL
C      XL=RATIO OF DISTANCE MEASURED FROM HOT GAS SIDE OF THE WALL
C      TEMPERATURE MEASURING LOCATION TO WALL THICKNESS
C      TG=MEAN TEMPERATURE OF HOT GAS
C      TWO=WALL TEMPERATURE, FUNCTION OF TIME, X=0.0
C      TWL=WALL TEMPERATURE, FUNCTION OF TIME, X=L
C      TC=MEAN TEMPERATURE OF THE COOLANT
C      WRAD=FREQUENCY OF TEMPERATURE OSCILLATIONS
C      OMDTG=RATIO OF THE AMPLITUDE OF THE WALL TEMPERATURE TO THE
C      AMPLITUDE OF THE SINUSOIDALLY DRIVEN HOT GAS TEMPERATURE
C      ALPFA=THERMAL DIFFUSIVITY
C      ETA=FREQUENCY AND WALL PROPERTY PARAMETER
C      HCA(1)=LOWER LIMIT OF COOLANT SIDE CONVECTIVE HEAT-TRANSFER
C      COEFFICIENT
C      HCA(3)=UPPER LIMIT OF COOLANT SIDE CONVECTIVE HEAT-TRANSFER
C      COEFFICIENT
C      FCT=TIME AVERAGED CONVECTIVE HEAT-TRANSFER COEFFICIENT ON
C      COOLANT SIDE OF THE WALL
C      FGT=TIME AVERAGED CONVECTIVE HEAT-TRANSFER COEFFICIENT ON HOT
C      GAS SIDE OF THE WALL
C      IJK=NUMBER OF ITERATIONS
C      R=RATIO OF CONVECTIVE HEAT-TRANSFER COEFFICIENTS
C      TCWA=CALCULATED COOLANT WALL TEMPERATURE
C      TEST1=HEAT FLUX TO THE COOLANT
C      TEST2=HEAT FLUX FROM THE HOT GAS
C
C *****
C      DIMENSION TCWA(300),WRAD(300),CMDTG(300),HCA(4),THETA(4)
C      EQUIVALENCE (PSIC,PHIC),(PSIG,PHIG)
C      REAL K,L,NUM1,NUM2,NUM,NEWERR
C *****
C      READ INPUT
C *****
C      1 READ(5,100) IRDG,ISTA,NR
C      READ(5,101) K,RHO,CC,L,XL,TG,TWC,TWL,TC
C      READ(5,101) (WRAD(I),OMDTG(I),I=1,NR)
C *****
C      PRINT TITLE AND INPUT
C *****
C      WRITE(6,102)
C      WRITE(6,103) IRDG,ISTA
C      ALPFA=K/(RHO*CC)
C      DO 2 I=1,NR
C      WRITE(6,104) I
C      WRITE(6,105)
C      WRITE(6,106)
C      WRITE(6,107) K,RHO,CC,L,XL,TG,TWC,TWL,TC,WRAD(I),OMDTG(I)
C *****
C      INITIALIZE STARTING VALUES FOR ITERATION
C *****
C      TCW=TWC
C      TCW=TC+10.
C      IGO=1
C *****
C      DEFINE HC BOUNDARY CONDITIONS AND CALCULATE R RATIO
C *****
C      5 R=(TG-TCW)/(TCW-TC)
C      FG=-K*(TCW-TG)/(L*(TG-TG))
C      FC=R*FG

```

```

C*****
C   CALCULATE AND COMPARE AMPLITUDE RATIOS
C*****
  ETA=SQRT(WRAD(I)/(2.0*ALPHA))
  ETAL=ETA*L
  ANG=2.0*(ETAL
  SANG= SIN(ANG)
  CANG= COS(ANG)
  EXPANG=EXP(ANG)
  THETA(2)=CMDTG(I)
  ANG1=ETAL*XL
  EXP1=EXP(ANG1)
  ANG2=ETAL*(2.0-XL)
  EXP2=EXP(ANG2)
  COS1=COS(ANG1)
  SIN1=SIN(ANG1)
  PHIC=K*ETA/HG
  PHIC=R*PHIC
  PGPPC=PHIC+PHIC
  PGPC2=PHIC*PHIC*2.0
  F=PHIC
  E=1.0-F
  PCP1=PHIC+1.0
  D=F*CANG+PCP1*SANG
  C=PCP1*CANG-PHIC*SANG
  B=(PGPPC-PGPC2)+EXPANG*((PGPPC+PGPC2)*CANG+(PGPPC+1.0)*SANG)
  A=1.0-PGPPC+EXPANG*((PGPPC+PGPC2)*SANG-(1.0+PGPPC)*CANG)
  DEL1=C*A-D*B
  DEL2=C*A+C*B
  DEL3=F*A-E*B
  DEL4=E*A+F*B
  NUM1=(DEL1*SIN1-DEL2*COS1)*EXP2
  NUM2=(DEL3*COS1-DEL4*SIN1)*EXP1
  NUM=NUM2-NUM1
  DEN=(DEL4*COS1+DEL3*SIN1)*EXP1-(DEL1*COS1+DEL2*SIN1)*EXP2
  A2PB2=A**2+B**2
  CON=SQRT(NUM**2+DEN**2)
  AMPDTG=CON/A2PB2
  DIFF=AMPDTG-OMDTG(I)
  CALL BALAN(TCW,IGD,DIFF)
  IF(IGD.LT.10) GO TO 9
  IJK=1
  TCWA(IJK)=TCW
  FCT=FCT
  FGT=FGT
  THETA(4)=AMPDTG
  TEST1=FCT*(TCW-TC)
  TEST2=FGT*(TG-TGW)
  TEST=TEST1/TEST2
  ERROR=1.-TEST
C*****
C   PRINT OUTPUT
C*****
  WRITE(6,109)
  WRITE(6,110)
  WRITE(6,111) TCWA(IJK),TEST1,TEST2,TEST,HCT,HGT,ERRCR,R,THETA(4)
2 CONTINUE
  GO TO 1
C*****

```

```

C      FORMAT STATEMENTS
C*****
100 FORMAT(2I2)
101 FORMAT(10E8.4)
102 FORMAT(12CH1CONVECTIVE HEAT-TRANSFER COEFFICIENTS FROM HARMONIC TEMPERATURE OSCILLATIONS - AMPLITUDE RATIO GIVEN )
103 FORMAT(18HCREADING NUMBER = ,I2,10X,18H STATION NUMBER = ,I2)
104 FORMAT(4HCRUN,I2)
105 FORMAT(6HCINPL1)
106 FORMAT(1HC,4X,1HK,8X,3HRHC,8X,2HCC,8X,1HL,9X,2HXL,8X,2HTG,7X,3HTWO,7X,3HTWL,7X,2HTC,7X,4HWRAD,6X,5HCOMDTG)
107 FORMAT(1HC,F8.6,4F10.4,4F10.1,2F10.4)
108 FORMAT(55HCITERATIONS EXCEED 50 )
109 FORMAT(7HCOUPL1)
110 FORMAT(1HC,3X,4HTCWA,5X,5HTEST1,5X,5HTEST2,6X,4HTEST,6X,3HHCT,7X,3HHGT,6X,5HERROR,7X,1HR,7X,5HTHETA)
111 FORMAT(1HC,F8.1,3F10.4,2F10.6,3F10.4)
112 FORMAT(55HC SOLUTION IS DIVERGING )
      END

```

#### \$1EFTC BALAN

```

      SUBROUTINE BALAN(X,K,Y)
      GO TO (1,2),K
1  X1=X
   Y1=Y
   X=X+X/10.
   K=2
   RETURN
2  X2=X
   Y2=Y
   IF(ABS(Y).LT.1.E-4)K=15
   X=(X2-Y1)/(Y2-Y1)*(-Y1)+X1
   X1=X2
   Y1=Y2
   RETURN
      END

```

### Program BL Output

CONVECTIVE HEAT-TRANSFER COEFFICIENTS FROM HARMONIC TEMPERATURE OSCILLATIONS - AMPLITUDE RATIO GIVEN

READING NUMBER = 1                      STATION NUMBER = 1

RUN 1

INPUT

K	RHO	CC	L	XL	TG	TWO	TWL	TC	WRAD	OMDTG
0.000207	1.2860	0.1170	0.0600	0.1667	960.0	658.0	658.0	570.6	1.2390	0.1538

OUTPUT

TCWA	TEST1	TEST2	TEST	HCT	HGT	ERROR	R	THETA
615.0	1.1344	0.1344	0.9998	0.002775	0.000445	0.0002	6.2350	0.1538

\*01\* UNITS, EOF.

REC= 00000 FILE= 00002

[illegible]

19

PROGRAM JCL - PHASE LAG ANGLE GIVEN

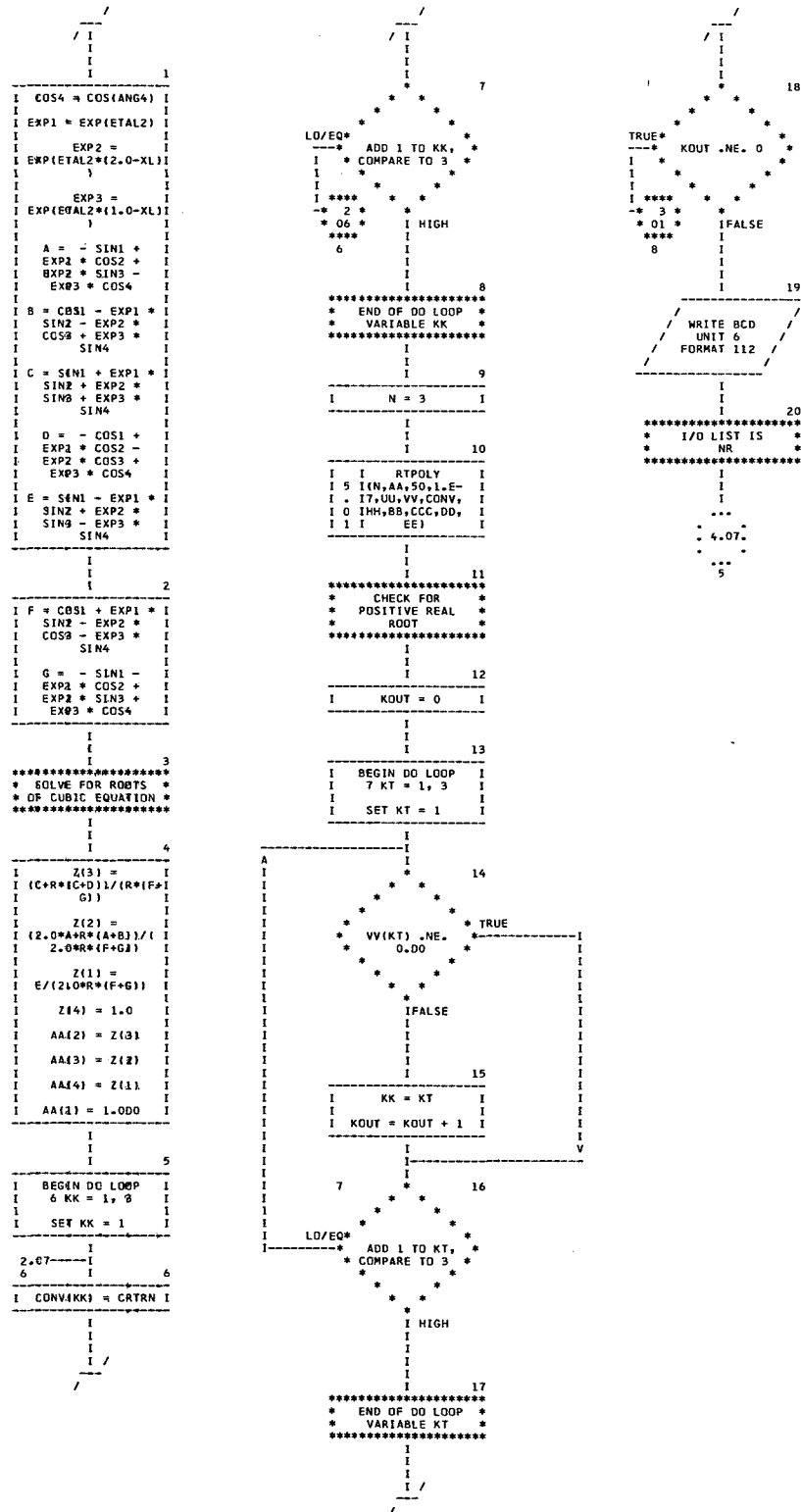


Figure 4. - Continued.



[illegible]

21



## SUBROUTINE RTPOLY

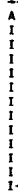
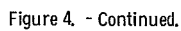


Figure 4. - Continued.



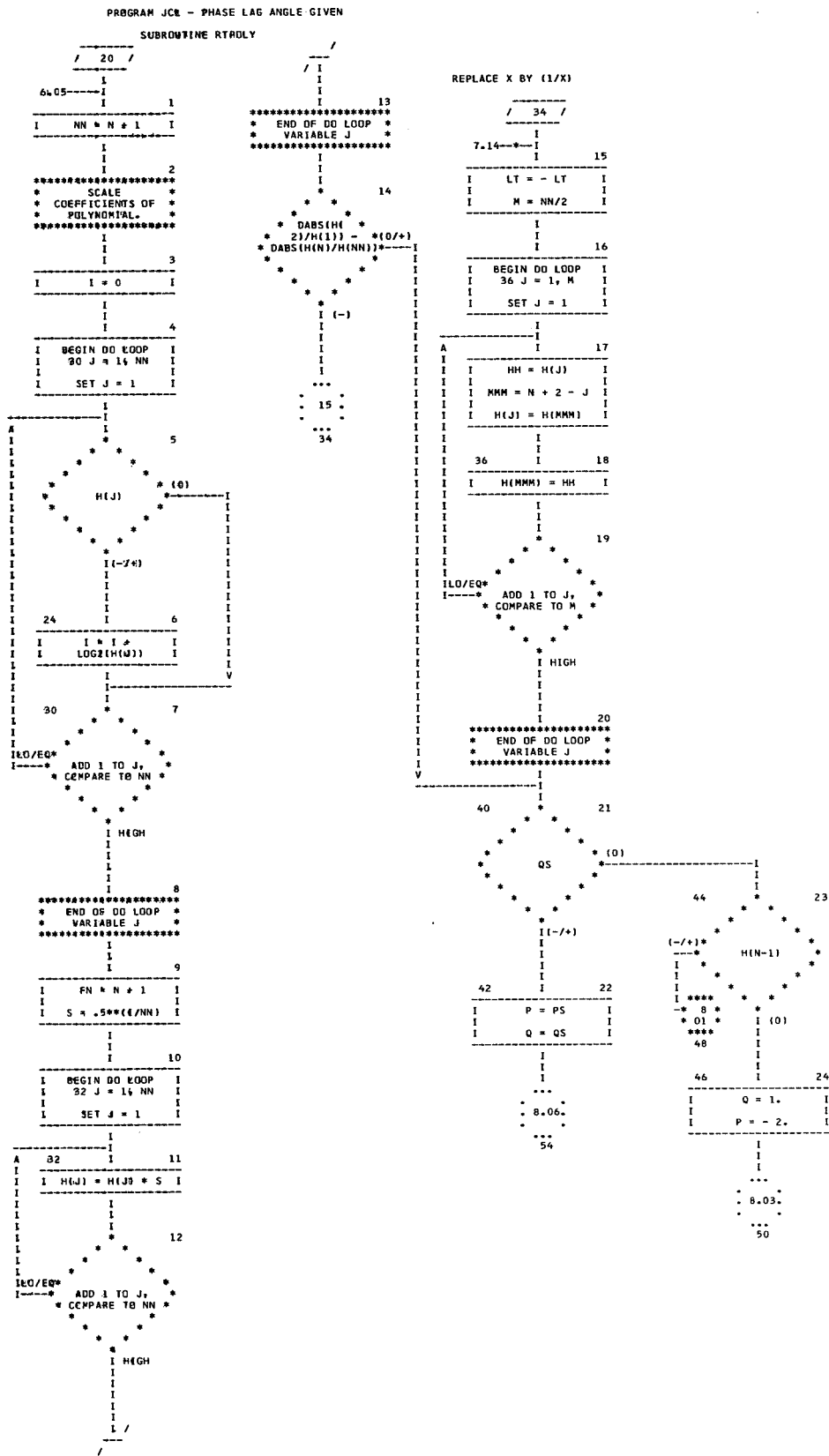


Figure 4. - Continued.

## SUBROUTINE RTPOLY

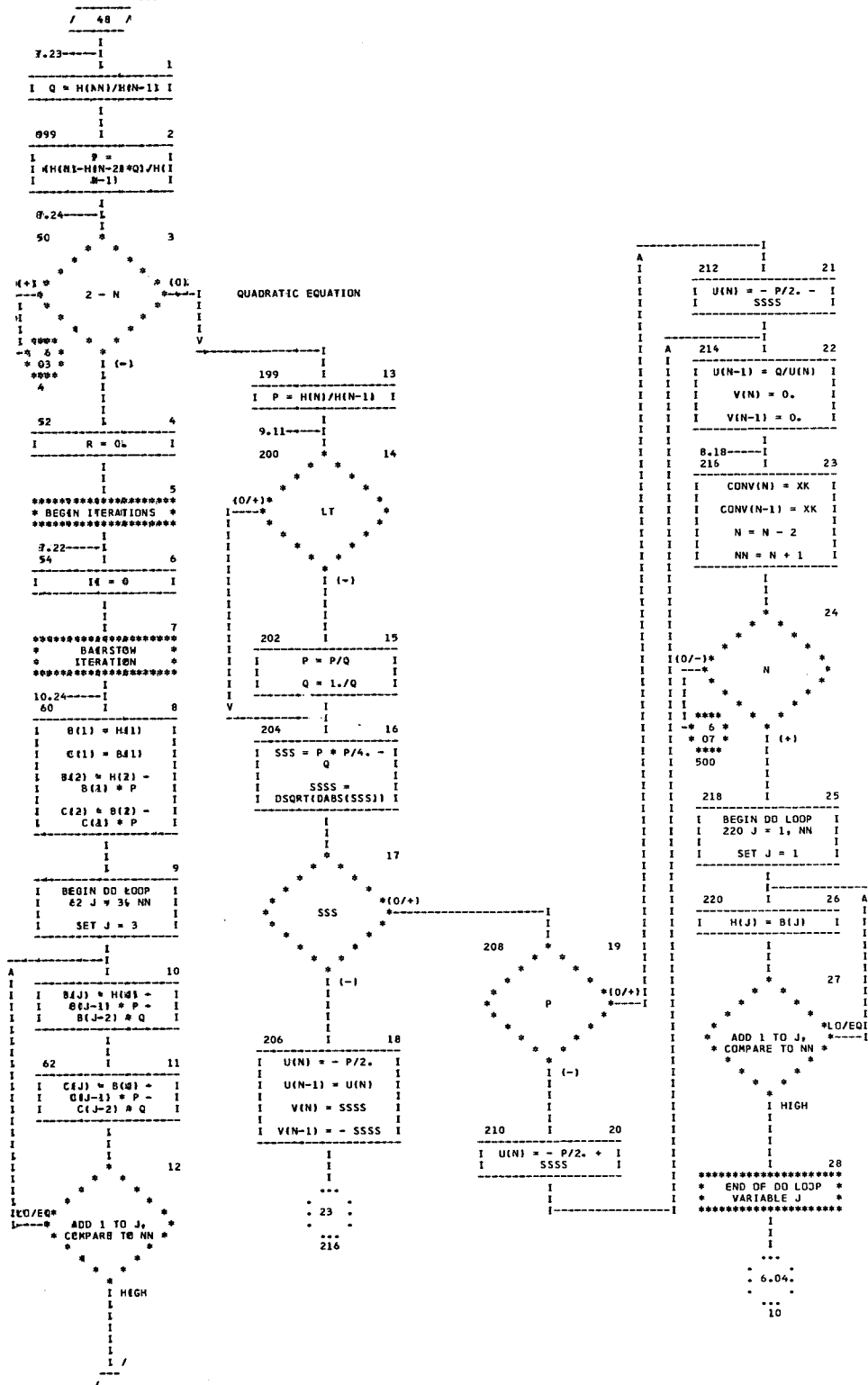


Figure 4. - Continued.

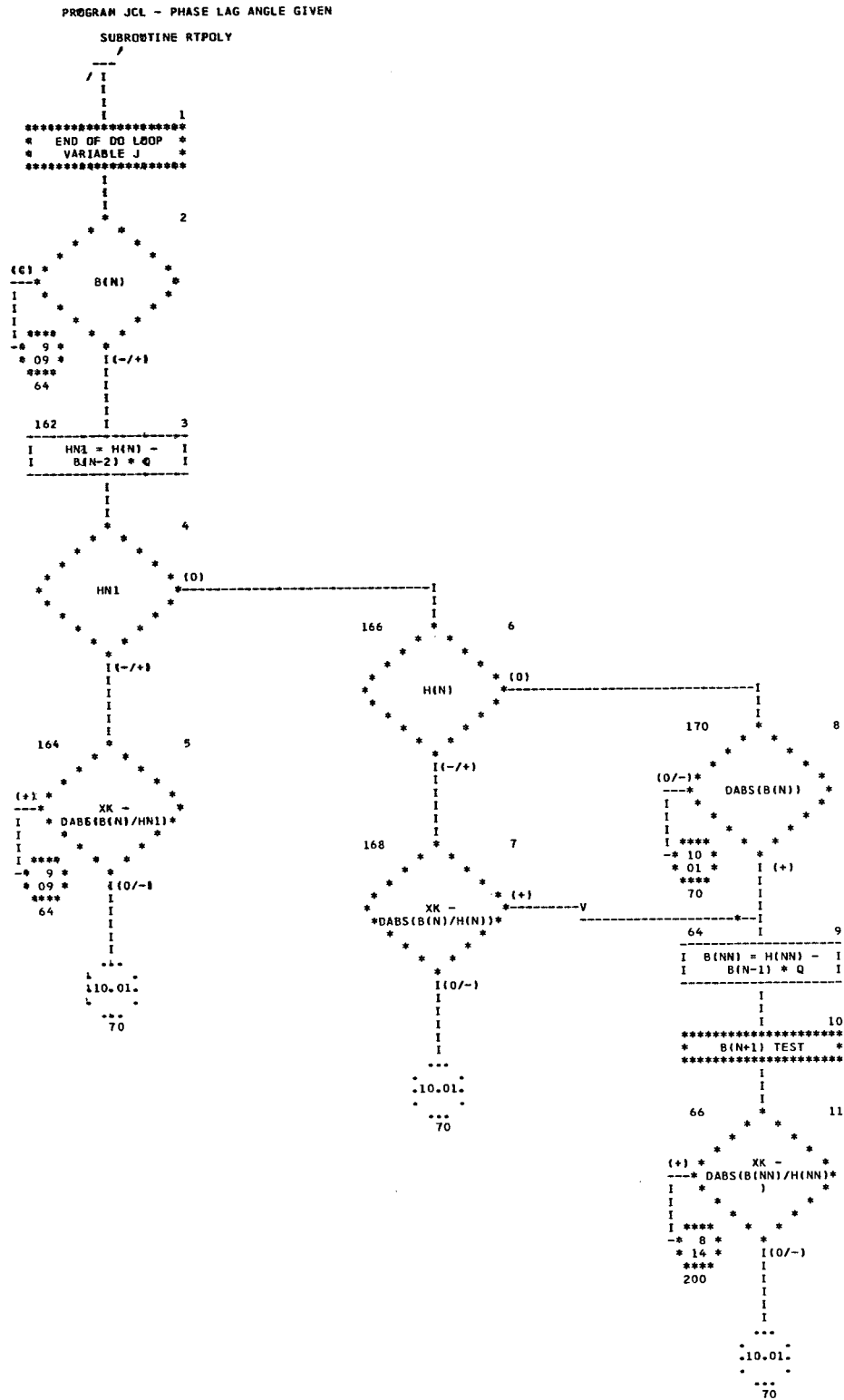


Figure 4. - Continued.



### NEWTON-RAPHSON ITERATION

### LINEAR EQUATION

1	$R = 1./R$	1
104		13
1	$U(N) = R$	1
1	$V(N) = 0.$	1
1	$CONV(N) = XK$	1
1	$N = N - 1$	1
1	$NN = N + 1$	1

I	BEGIN DO LOOP	I
I	108 J = 1, NN	I
I		I
I	SET J = 1	I

[illegible]

```

      / 78 /
      -----
          I
10.09-----I
          I
19
-----
I      P = P - 2.      I
I
I      Q = Q * (Q + 1.) I

```

[illegible]

28

# Program JCL

\$IEFTC JCL

```

C
C
C *****
C   CONVECTIVE HEAT-TRANSFER COEFFICIENTS FROM HARMONIC TEMPERATURE
C   OSCILLATIONS - PHASE LAG ANGLE GIVEN
C *****
C
C   IRDG=READING NUMBER
C   ISTA=STATION NUMBER
C   NR=NUMBER OF DATA POINTS TO BE COMPUTED
C   K=THERMAL CONDUCTIVITY OF WALL MATERIAL
C   RHO=DENSITY OF WALL MATERIAL
C   CC=SPECIFIC HEAT OF WALL MATERIAL
C   L=THICKNESS OF WALL MATERIAL
C   XL=RATIO OF DISTANCE MEASURED FROM HOT GAS SIDE OF THE WALL
C       TEMPERATURE MEASURING LOCATION TO WALL THICKNESS
C   TG=MEAN TEMPERATURE OF HOT GAS
C   TGH=WALL TEMPERATURE,FUNCTION OF DISTANCE
C   TC=MEAN TEMPERATURE OF THE COOLANT
C   WRADA=FREQUENCY OF TEMPERATURE OSCILLATIONS
C   PHIRA=PHASE LAG ANGLE BETWEEN THE DRIVING GAS TEMPERATURE AND THE
C         RESPONDING WALL TEMPERATURE
C   ALPHA=THERMAL DIFFUSIVITY
C   ETA=FREQUENCY AND WALL PROPERTY PARAMETER
C   GR=CUBIC EQUATION CHECK OF ROOTS, SHOULD APPROXIMATE ZERO
C   HCT=TIME AVERAGED CONVECTIVE HEAT-TRANSFER COEFFICIENT ON
C       COOLANT SIDE OF THE WALL
C   HGT=TIME AVERAGED CONVECTIVE HEAT-TRANSFER COEFFICIENT ON HOT
C       GAS SIDE OF THE WALL
C   IJK=NUMBER OF ITERATIONS
C   R=RATIO OF CONVECTIVE HEAT-TRANSFER COEFFICIENTS
C   PSIG=CONVECTIVE HEAT-TRANSFER PARAMETER ON THE HOT GAS SIDE OF
C       THE WALL
C   PSIC=CONVECTIVE HEAT-TRANSFER PARAMETER ON THE COOLANT SIDE OF
C       THE WALL
C   TCH=CALCULATED COOLANT WALL TEMPERATURE
C   TEST1=HEAT FLUX TO THE COOLANT
C   TEST2=HEAT FLUX FROM THE HOT GAS
C   CONV=CONVERGENCE CRITERION USED FOR EACH ROOT
C
C *****
C   DIMENSION WRADA(100),PHIRA(100),TCH(100),Z(4),CCNV(4)
C   DOUBLE PRECISION HH(4),BB(4),CCC(4),DD(4),EE(4),AA(4),UU(4),VV(4)
C   REAL L,K
C   DATA CRTRN/1.E-5/
C   PI=3.1415926
C   PID180=PI/180.
C *****
C   READ INPUT
C *****
1 READ(5,100) IRDG,ISTA,NR
  READ(5,101) K,RHO,CC,L,XL,TG,TGH,TC

```

```

      READ(5,101) (WRADA(I),PHIRA(I),I=1,NR)
C*****
C      PRINT TITLE AND INPUT
C*****
      WRITE (6,102)
      WRITE(6,103) IRDG,ISTA
      DO 5 JJ=1,NR
      WRITE(6,104) JJ
      WRITE(6,105)
      WRITE(6,106)
      WRITE(6,107) K,RHO,CC,L,XL,TG,TGW,TC,WRADA(JJ),PHIRA(JJ)
C*****
C      INITIALIZE STARTING VALLES FOR ITERATION
C*****
      IJK=1
      TCWA(IJK)=TGW
      TCW=TCW
      WRAC=WRADA(JJ)
      PHI=PHIRA(JJ)
C*****
C      CALCULATE R RATIO
C*****
      Z R=(TG-TGW)/(TCW-TC)
      ALPA=A/(RHO*CC)
      X=L*XL
      ETA=SQRT(WRAD/(2.0*ALPHA))
      ETAL=ETA*L
      ETAL2=ETAL*2.0
      ETAX=ETAL*XL
      ANG1=PI+ETAX
      SIN1=SIN(ANG1)
      COS1=COS(ANG1)
      ANG2=ANG1-ETAL2
      SIN2=SIN(ANG2)
      COS2=COS(ANG2)
      ANG3=PI-ETAX
      SIN3=SIN(ANG3)
      COS3=COS(ANG3)
      ANG4=ANG3+ETAL2
      SIN4=SIN(ANG4)
      COS4=COS(ANG4)
      EXP1=EXP(ETAL2)
      EXP2=EXP(ETAL2*(2.0-XL))
      EXP3=EXP(ETAL2*(1.0-XL))
      A=-SIN1+EXP1*COS2+EXP2*SIN3-EXP3*COS4
      B=COS1-EXP1*SIN2-EXP2*COS3+EXP3*SIN4
      C=SIN1+EXP1*SIN2+EXP2*SIN3+EXP3*SIN4
      D=-COS1+EXP1*COS2-EXP2*COS3+EXP3*COS4
      E=SIN1-EXP1*SIN2+EXP2*SIN3-EXP3*SIN4
      F=COS1+EXP1*SIN2-EXP2*COS3-EXP3*SIN4
      G=-SIN1-EXP1*COS2+EXP2*SIN3+EXP3*COS4
C*****
C      SOLVE FOR ROOTS OF CUBIC EQUATION
C*****
      Z(3)=(C+R*(C+D))/(R*(F+G))
      Z(2)=(2.0*A+R*(A+B))/(2.0*R*(F+G))
      Z(1)=E/(2.0*R*(F+G))
      Z(4)=1.0
      AA(2)=Z(3)

```

```

      AA(2)=Z(2)
      AA(4)=Z(1)
      AA(1)=1.0DC
      DO 6 KK=1,3
6     CONV(KK)=CRRN
      N=3
      CALL RTPOLY(N,AA,50,1.E-7,UU,VV,CONV,HH,BB,CCC,DD,EE)
C *****
C     CHECK FOR POSITIVE REAL ROOT
C *****
      KOUT=C
      DO 7 KT=1,3
      IF(VV(KT).NE.0.D0) GO TO 7
      KK=KT
      KOUT=KOUT+1
7     CONTINUE
      IF(KOUT.NE.0) GO TO 8
      WRITE(6,112) NR
      GO TO 5
8     IF(KOUT.EQ.1) GO TO 11
      KOUT=C
      DO 9 KT=1,3
      IF(UU(KT).LE.0.DC) GO TO 9
      KK=KT
      KOUT=KOUT+1
9     CONTINUE
      IF(KOUT.EQ.1) GO TO 12
10    WRITE(6,113) NR
      GO TO 5
11    IF(UU(KK).LE.0.DC) GO TO 10
12    REAL2=LL(KK)
      REAL1=REAL2*R
      GR=((REAL2+Z(3))*REAL2+Z(2))*REAL2+Z(1)
      HCT=(K*ETA)/REAL2
      HGT=(K*ETA)/REAL1
      PSIC=REAL2
      PSIG=REAL1
C *****
C     CALCULATE AND COMPARE COOLANT WALL TEMPERATURES
C *****
      IJK=IJK+1
      TCWA(IJK)=TGW-HGT*L*(TG-TGW)/K
      TCW=TCWA(IJK)
      TEST1=HCT*(TCW-TC)
      TEST2=HGT*(TG-TGW)
      TEST=TEST1/TEST2
      ERROR=1.0-TEST
      IF(ABS(ERROR).LT..01) GO TO 4
      TCWA(IJK)=(TCWA(IJK-1)+TCWA(IJK))/2.0
      TCW=TCWA(IJK)
      IF(IJK.LT.50) GO TO 2
      WRITE(6,108)
      GO TO 5
4     R=(TG-TGW)/(TCW-TC)
C *****
C     PRINT OUTPUT
C *****
      WRITE(6,109)
      WRITE(6,110)

```

```

        WRITE(6,111) TCWA(IJK),TEST1,TEST2,TEST,HCT,HGT,ERRCR,R,PS IC,PS IG,
1GR
5 CONTINUE
        WRITE(6,114)
        GO TO 1
C *****
C      FORMAT STATEMENTS
C *****
100 FORMAT(3I2)
101 FORMAT(10E8.4)
102 FORMAT(12CH1CONVECTIVE HEAT-TRANSFER CCEFFICIENTS FROM HARMONIC TE
      IMPERATURE OSCILLATIONS - PHASE LAG ANGLE GIVEN )
103 FORMAT(18F-CREADING NUMBER = ,I2,10X,18H STATION NUMBER = ,I2)
104 FORMAT(4HCRUN,I2)
105 FORMAT(6HCINPUT)
106 FORMAT(1HC,4X,1HK,8X,3HRHC,8X,2HCC,8X,1HL,9X,2HXL,8X,2HTG,7X,3HTGW
      1,8X,2HTC,6X,5HWRADA,5X,5HPHIRA)
107 FORMAT(1H0,F8.6,4F10.4,3F10.1,2F10.4)
108 FORMAT(55H-ITERATIONS EXCEED 50 )
109 FORMAT(7HOUTPUT)
110 FORMAT(1HC,4X,3HTCW,5X,5HTEST1,5X,5HTEST2,6X,4HTEST,6X,3HHCT,7X,3H
      1HGT,6X,5HERKOR,7X,1HR,8X,4HPSIC,6X,4HPSIG,7X,2HGR)
111 FORMAT(1HC,F8.1,3F10.4,2F10.6,5F10.4)
112 FORMAT(40H-ERROR IN SUBR RTPOLY FOR DATA PCINT NO. I5)
113 FORMAT(63H-0A UNIQUE POSITIVE REAL RCCT CANNOT BE FOUND FOR DATA PO
      INT NO. I5)
114 FORMAT(1H1)
      END

```

# \$IEFTC POLRT

```

      SUBROUTINE RTPOLY(N,A,L,F,U,V,CONV,H,B,C,D,E)
C      N      ORDER OF INPUT POLYNOMIAL
C      A      COEFFICIENTS OF INPUT POLYNOMIAL IN DESCENDIN ORDER
C      L      MAXIMUM NUMBER OF ITERATION FOR EACH RCCT
C      F      DESIRED TOLERANCE (REMAINDER / CONSTANT TERM)
C      U      REAL PART OF ROOT
C      V      IMAGINARY PART OF RCCT
C      CONV   CONVERGENCE CRITERION USED FOR EACH ROOT
C             IF AFTER L ITERATIONS CONVERGENCE WITHIN F FAILS,
C             THE TOLERANCE IS RELAXED BY 10.
C      H      WORKING STORAGE
C      B      WORKING STORAGE
C      C      WORKING STORAGE
C      D      WORKING STORAGE
C      E      WORKING STORAGE
      DIMENSION A(40),U(40),V(40),CCNV(40),H(40),B(40),C(40),D(40),E(40)
      DOUBLE PRECISION A,U,V,H,B,C,D,E
      DOUBLE PRECISION P,Q,R,S,PS,CS,PT,QT,HH,HN1,XK,SSS,SSSS
      NSAVE = N
      NN = N+1
      DO 1 I = 1,NN
1 H(I) = A(I)
      XK = F
      LT = 1
C      EXTRACT ZERO ROOTS
2 IF(H(NN)) 4,3,4
3 U(N) = C.
  V(N) = C.
  CONV(N) = XK
  N = N-1

```

```

      NN = N+1
      GO TO 2
4  IF(N) 500,500,10
C  INITIALIZE P,Q,ETC.
10  S = 0.
      PS = C.
      QS = 0.
      PT = 0.
      QT = 0.
      XK = F
      IF (N-1) 500,12,20
12  R = -F(2)/H(1)
      GO TO 100
20  NN = N+1
C  SCALE COEFFICIENTS OF POLYNOMIAL.
      I=0
      DO 30 J = 1,NN
      IF(H(J)) 24,30,24
24  I=I+LOG2(H(J))
30  CONTINUE
      FN = N + 1
      S=.5** (1/NN)
      DO 32 J = 1,NN
32  H(J)=H(J)*S
      IF(DABS(H(2)/H(1)) - DABS(H(N)/H(NN))) 34,40,40
C  REPLACE X BY (1/X)
34  LT = - LT
      M = NN/2
      DO 36 J = 1, M
      HH = H(J)
      MMM =N+2-J
      H(J) = H(MMM)
36  H(MMM) = HH
40  IF(QS) 42,44,42
42  P = PS
      Q = QS
      GO TO 54
44  IF(H(N-1)) 46,46,48
46  Q = 1.
      P = -2.
      GO TO 50
48  Q = H(NN)/H(N-1)
599 P = (H(N)-H(N-2)*Q)/H(N-1)
50  IF(2-N) 52,199,4
52  R = C.
C  BEGIN ITERATIONS
54  II = 0
C  BAIRSTOW ITERATION
60  B(1) = H(1)
      C(1) = B(1)
      B(2) = H(2) - B(1)*P
      C(2) = B(2) - C(1)*P
      DO 62 J = 3,NN
      B(J) = H(J) - B(J-1)*P - B(J-2)*Q
62  C(J) = B(J) - C(J-1)*P - C(J-2)*Q
      IF(B(N)) 162,64,162
162  HN1 = H(N) - B(N-2) *Q
      IF(HN1) 164,166,164
164  IF(XK - DABS(B(N)/HN1)) 70,70,64
166  IF(H(N)) 168,170,168
168  IF(XK - DABS(B(N)/H(N))) 70,70,64
170  IF(DABS(B(N))) 70,70,64
      64 B(NN) = H(NN) - B(N-1)*Q
C  B(N+1) TEST

```

```

IB400310
IB400320
IB400330
IB400340
IB400350
IB400360
IB400370
IB400380
IB400390
IB400400
IB400410
IB400420
IB400430
IB400440
IB400450
IB400460
IB400470
IB400480
IB400490
IB400500
IB400510
IB400520
IB400530
IB400540
IB400550
IB400560
IB400570
IB400580
IB400590
IB400600
IB400610
IB400620
IB400630
IB400640
IB400650
IB400660
IB400670
IB400680
IB400690
IB400700
IB400710
IB400720
IB400730
IB400740
IB400750
IB400760
IB400770
IB400780
IB400790
IB400800
IB400810
IB400820
IB400830
IB400840
IB400850
IB400860
IB400870
IB400880
IB400890
IB400900
IB400910
IB400920
IB400930
IB400940

```

66 IF(XK - DABS(B(NN)/H(NN))) 70,70,200	IB40095C
C NEWTON-RAPHSON ITERATION	IB40096C
70 D(1) = H(1)	IB40097C
E(1) = D(1)	IB40098C
DO 72 J = 2, NN	IB40099C
C(J) = H(J) + D(J-1)*R	IB40100C
72 E(J) = D(J) + E(J-1)*R	IB40101C
IF(XK - DABS(D(NN)/H(NN))) 74,74,100	IB40102C
74 C(N) = -C(N-1)*P - C(N-2)*Q	IB40103C
SS = C(N-1)*C(N-1) - C(N)*C(N-2)	IB40104C
IF(SS) 76,78,76	IB40105C
76 P = P + (B(N)*C(N-1)-B(NN)*C(N-2))/SS	IB40106C
Q = Q + (-B(N)*C(N) + B(NN)*C(N-1))/SS	IB40107C
GO TO 80	IB40108C
78 P = P - 2.	IB40109C
Q = Q*(Q + 1.)	IB40110C
80 IF(E(N)) 84,82,84	IB40111C
82 R = R - 1.	IB40112C
GO TO 86	IB40113C
84 R = R - D(NN)/E(N)	IB40114C
86 II = II + 1	IB40115C
IF(II - L) 60,90,90	IB40116C
90 PS = PT	IB40117C
QS = QT	IB40118C
PT = P	IB40119C
QT = Q	IB40120C
92 XK = 1C.*XK	IB40121C
GO TO 24	IB40122C
C LINEAR EQUATION	IB40123C
100 IF(LT) 102,104,104	IB40124C
102 R = 1./R	IB40125C
104 U(N) = R	IB40126C
V(N) = 0.	IB40127C
CONV(N) = XK	IB40128C
N = N-1	IB40129C
NN = N + 1	IB40130C
IF(N) 100,500,106	IB40131C
106 DO 108 J = 1, NN	IB40132C
108 H(J) = D(J)	IB40133C
GO TO 10	IB40134C
C QUADRATIC EQUATION	IB40135C
199 P = H(N)/H(N-1)	IB40136C
200 IF(LT) 202,204,204	IB40137C
202 P = P/Q	IB40138C
Q = 1./Q	IB40139C
204 SSS = P*P/4. - Q	IB40140C
SSSS = DSQRT(DABS(SSS))	IB40141C
IF(SSS) 206,208,208	IB40142C
206 U(N) = - P/2.	IB40143C
U(N-1) = U(N)	IB40144C
V(N) = SSSS	IB40145C
V(N-1) = - SSSS	IB40146C
GO TO 216	IB40147C
208 IF(P) 210,212,212	IB40148C
210 U(N) = - P/2. + SSSS	IB40149C
GO TO 214	IB40150C
212 U(N) = - P/2. - SSSS	IB40151C
214 U(N-1) = Q/U(N)	IB40152C
V(N) = 0.	IB40153C
V(N-1) = 0.	IB40154C
216 CONV(N) = XK	IB40155C
CONV(N-1) = XK	IB40156C
N = N-2	IB40157C
NN = N + 1	IB40158C
IF(N) 100,500,218	IB40159C
218 DO 220 J = 1,NN	IB40160C



```

22C H(J) = B(J)
GO TO 10
C RESTORE N, RETURN.
50C N = NSAVE
RETURN
END

```

```

IB40161C
IB40162C
IB40163C
IB40164C
IB40165C
IB40166C

```

## Program JCL Output

CONVECTIVE HEAT-TRANSFER COEFFICIENTS FROM HARMONIC TEMPERATURE OSCILLATIONS - PHASE LAG ANGLE GIVEN

READING NUMBER = 1                  STATION NUMBER = 1

RUN 1

INPUT

K	RHO	CC	L	XL	TG	TGW	TC	WRADA	PHIRA
0.000207	0.2860	0.1170	0.0600	0.1667	960.0	658.0	570.6	1.2380	0.7673

OUTPUT

TCW	TEST1	TEST2	TEST	HCT	HGT	ERRCR	R	PSIC	PSIG	GR
624.6	0.1146	0.1152	0.9949	0.002121	0.000381	0.0051	5.5903	0.9764	5.4305	-0.0000

Lewis Research Center,  
National Aeronautics and Space Administration,  
Cleveland, Ohio, July 13, 1970,  
129-04.

## APPENDIX - SYMBOLS

Machine code	Engineering symbol	
ALPHA	$\alpha$	thermal diffusivity, $K/\rho C$ , $\text{in.}^2/\text{sec}$ ; $\text{m}^2/\text{sec}$
CC	c	specific heat of wall material, $\text{Btu}/(\text{lbm})(^\circ\text{R})$ ; $\text{J}/(\text{kg})(\text{K})$
ERROR	---	$1.0 - (\text{TEST1})/(\text{TEST2})$
ETA	$\eta$	frequency and wall property parameter, $1/\text{in.}$ ; $1/\text{m}$
GR	---	cubic equation check of roots, equals zero for correct solution
HCA(1)	---	lower limits of the coolant-side convective heat-transfer coefficient
HCA(3)	---	upper limits of the coolant-side convective heat-transfer coefficient
HCT	$h_c$	time averaged convective heat-transfer coefficient on the coolant side of the wall, $\text{Btu}/(\text{in.}^2)(\text{sec})(^\circ\text{R})$ ; $\text{W}/(\text{m}^2)(\text{K})$
HGT	$h_G$	time averaged convective heat-transfer coefficient on hot-gas side of wall, $\text{Btu}/(\text{in.}^2)(\text{sec})(^\circ\text{R})$ ; $\text{W}/(\text{m}^2)(\text{K})$
IJK	---	number of iterations
IRDG	---	reading number
ISTA	---	station number
K	K	thermal conductivity of wall material, $\text{Btu}/(\text{in.})(\text{sec})(^\circ\text{R})$ ; $\text{J}/(\text{m})(\text{sec})(\text{K})$
L	L	thickness of wall material, $\text{in.}$ ; $\text{m}$
NR	---	number of readings to be computed
OMDTG	$\theta/\Delta T_G$	ratio of amplitude of wall temperature to amplitude of sinusoidally driving hot-gas temperature
PHIRA	$\phi$	phase-lag angle between driving gas temperature and responding wall temperature, $\text{rad}$
R	R	ratio of convective heat-transfer coefficients, $h_c/h_G$
REAL1	$\psi_G$	convective heat-transfer parameter on hot-gas side of wall (JCL program), $K\eta/h_G$

Machine code	Engineering symbol	
REAL2	$\psi_c$	convective heat-transfer parameter on coolant side of the wall, $K\eta/h_c$
RHO	$\rho$	density of wall material, lbm/in. <sup>3</sup> ; g/m <sup>3</sup>
XL	$x/L$	ratio of distance measured from the hot-gas side of wall to wall temperature measuring location to the wall thickness
TC	$\bar{T}_c$	mean temperature of the coolant, °R; K
TCW	$T_{cw}$	calculated coolant wall temperature (JCL program), °R; K
TCWA	$T_{cw}$	calculated coolant wall temperature (BL program), °R; K
TEST1	$q_c$	heat flux to coolant, Btu/(in. <sup>2</sup> )(sec); W/m <sup>2</sup>
TEST2	$q_G$	heat flux from hot gas, Btu/(in. <sup>2</sup> )(sec); W/m <sup>2</sup>
TG	$\bar{T}_G$	mean temperature of hot gas, °R; K
TGW	$T(x, \tau)$	wall temperature, function of distance (measured into wall from hot surface) and time (JCL program), °R; K
TWL	$T(L, \tau)$	wall temperature, function of time at $x = L$ (BL program), °R; K
TWO	$T(O, \tau)$	wall temperature, function of time at $x = 0$ (BL program), °R; K
WRAD	$f$	frequency of temperature oscillations (BL program), rad/sec
WRADA	$f$	frequency of temperature oscillations (JCL program), rad/sec

## REFERENCE

1. Huff, Ronald G.: Convective Heat-Transfer Coefficients from a Solution of the Conduction Equation for a Wall Separating Two Fluids, One Having an Oscillating Temperature. NASA TN D-5520, 1969.

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